



Ongoing Spanish Team activity on HPT

# High temperature heat pumps for industry decarbonisation

José Ignacio Linares // ICAI – Comillas Pontifical University Madrid, 11th November 2024





Ciemat Centro de Investigaciones Energéticas, Medioambientales y Tecnológicas

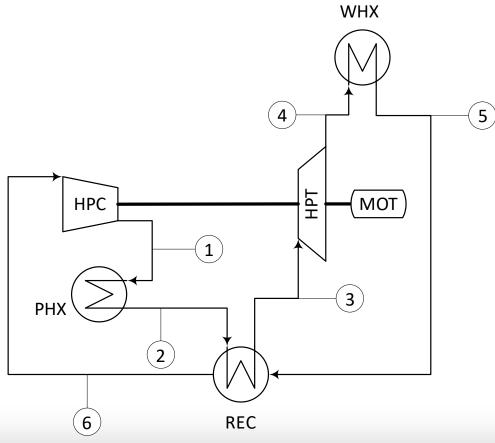








### **Reverse Brayton cycle for heat pumps**



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- Reverse Brayton cycle (the opposite to a closed-cycle gas turbine)
- Turbine replaces the valve of typical reverse Rankine cycles
- Turbocompressors are already used in large Rankine cycles
- PHX (gas cooler) is in the high pressure side
- WHX (gas heater) is in the low pressure side

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CO<sub>2</sub> is chosen as working fluid



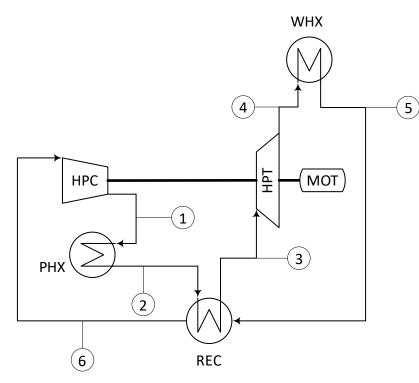






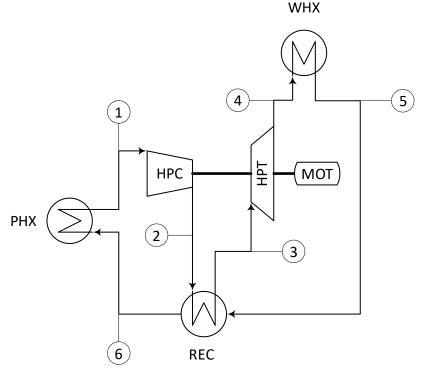


### **Reverse Brayton cycle for heat pumps**



- PHX is in the high pressure side
- Best option if no thermal storage is needed

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- PHX is in the low pressure side
- Best option if thermal storage is needed







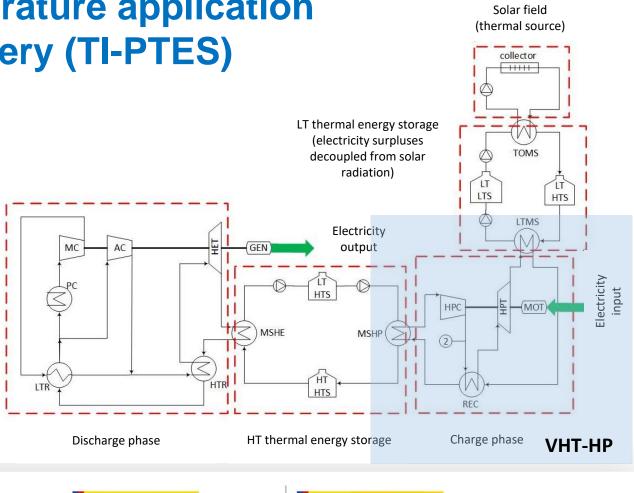




# Very high temperature application Carnot battery (TI-PTES)

- Heat pump is fed from a PTC solar field (400 °C/300 °C), supplying useful heat at (600 °C/400 °C)
- HT thermal energy storage works as if a heliostat field is feeding, whereas the heat comes from a PTC field

[Linares et al., Energies 16(9) 2023, 3871]







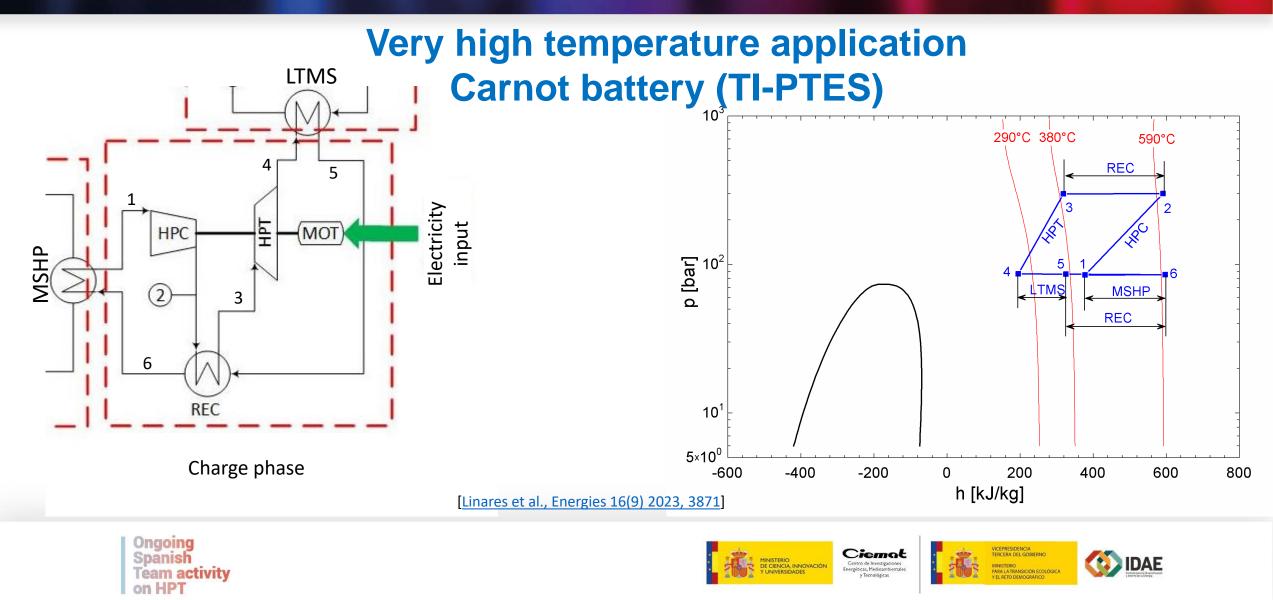










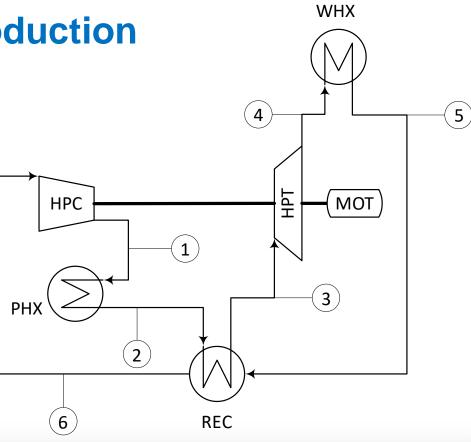






# **Industrial application Compressed water production**

- Application to beverage sector ٠
- Product: compressed water 210 °C/ 120 °C •
- Source: waste heat arriving at the WHX at 100 °C or 50 °C (two • cases)
- No thermal storage is required ٠







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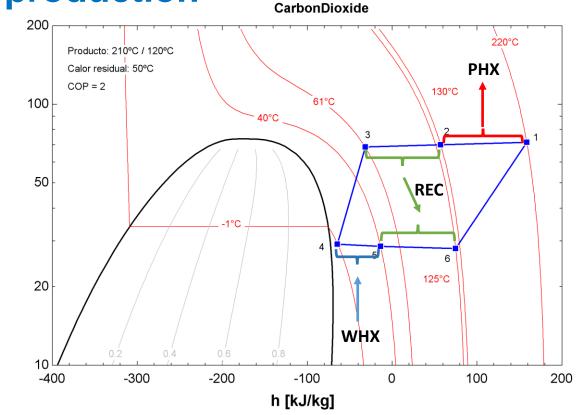




### **Industrial application Compressed water production**

P [bar]

- Waste heat arriving at the WHX at 50 °C
- Product (PHX) •
  - Liquid water inlet at 120 °C ٠
  - Liquid water outlet at 210 °C •
- COP = 2
- Waste heat (WHX) •
  - Liquid water inlet at 50 °C •
  - Liquid water outlet at 9 °C ٠
  - Water leaving WHX might be used as heat sink of chillers ٠







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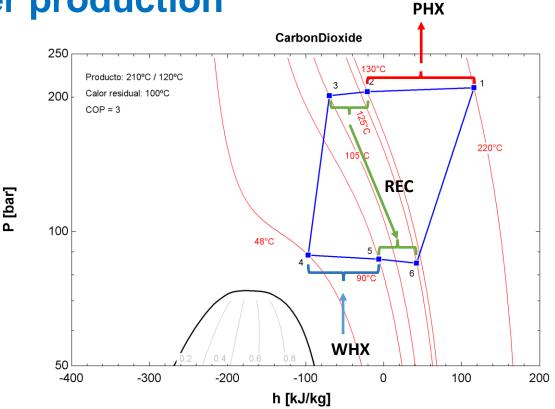






# Industrial application Compressed water production

- Waste heat arriving at the WHX at 100 °C
- Product (PHX)
  - Liquid water inlet at 120 °C
  - Liquid water outlet at 210 °C
- COP = 3
- Waste heat (WHX)
  - Liquid water inlet at 100 °C
  - Liquid water outlet at 58 °C
  - Water leaving WHX might be used for warming purposes



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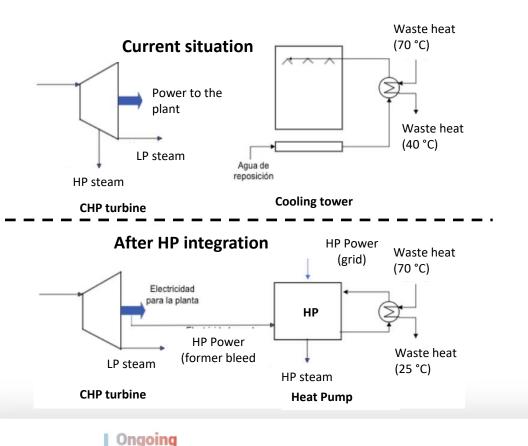








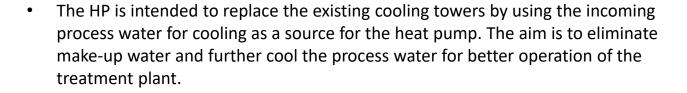
### Industrial application Steam production (10 – 12 bara)



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- The HP will produce process steam, which replaces the steam currently extracted from the CHP steam turbine. The electricity produced by the steam that now is not extracted from the turbine, partly offsets the electricity consumption of the pump.
- The HP would be placed next to the cooling towers, to take advantage of the existing process water piping connections. A thermal oil loop is required to transfer the heat from the PHX to the steam production system (ECO-EV-SH).
- Two designs have been proposed, one for low process flow rate (12 bara) and another one for high process flow rate (10 bara). The sizing is done for the highest mass flow rate.

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#### A. González-Alonso, Mater Thesis Dissertation, 2024





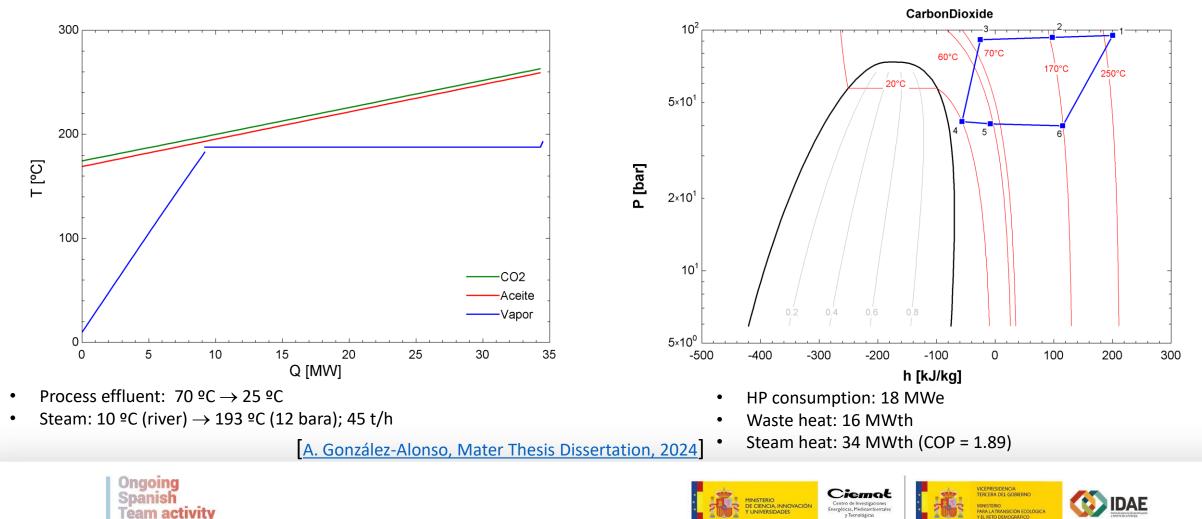




on HP1



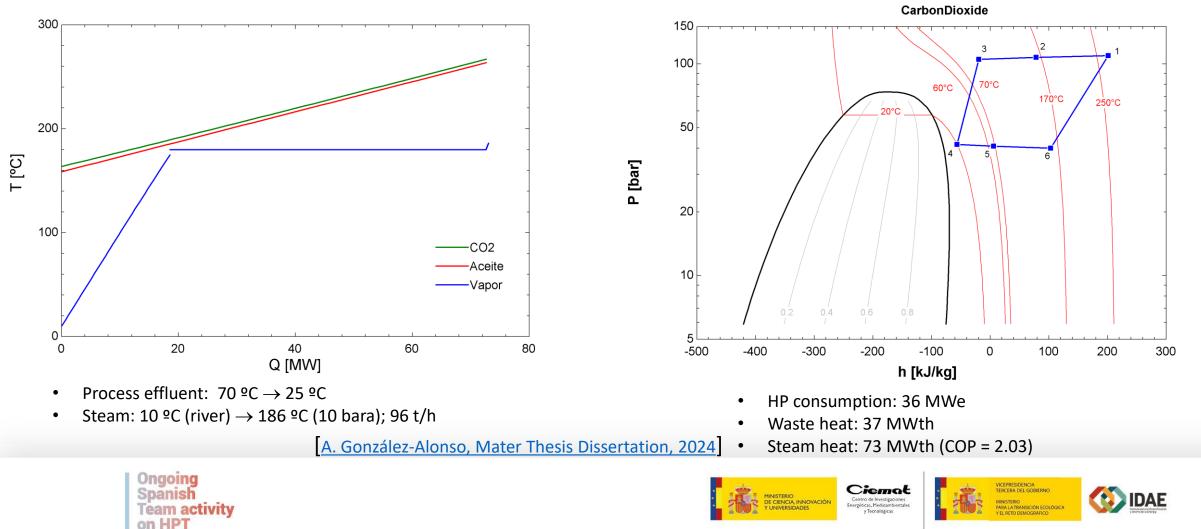
### Industrial application. Steam production (12 bara)







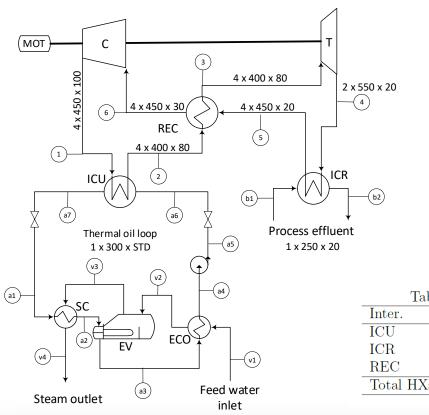
### Industrial application. Steam production (10 bara)







### **Industrial application. Steam production**



#### **HP sizing**

- No. of pipes x DN x Schedule •
- Heat exchangers: Width (m) x Depth (m) x Height (m) •
  - REC: 2 units: 0.6 x 6 x 2.5 ٠
  - ICU: 0.6 x 8 x 5 ٠
  - ICR: 0.6 x 7 x 2 ٠
  - Theorical dimensions (no connection ports) ٠

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Tabla 2: Inversión requerida por los intercambiadores						
UA $[W/(m^2K)]$	PEC [€]	ONSC [€]	FCI [€]			
4.341.593	5.030.473	6.539.614	8.174.518			
2.207.637	3.020.128	3.926.166	4.907.708			
5.087.890	5.669.939	7.370.920	9.213.651			
	13.720.539	17.836.701	22.295.876			
	$\frac{\text{UA [W/(m^2 \text{K})]}}{4.341.593}$ 2.207.637	UA $[W/(m^2K)]$ PEC [€]4.341.5935.030.4732.207.6373.020.1285.087.8905.669.939	UA $[W/(m^2K)]$ PEC $[\in]$ ONSC $[\in]$ 4.341.5935.030.4736.539.6142.207.6373.020.1283.926.166			

Total investment: 608 €/kWth

Tabla 3: Inversión requerida por equipos rotativos						
	Potencia [MW]	PEC [€]	ONSC [€]	FCI [€]		
Compresor	$57,\!851$	6.214.692	8.079.100	10.098.875		
Turbina	22,067	1.020.367	1.326.477	1.658.096		
Motor	35,784	3.493.448	4.541.482	5.676.853		
Total		10.728.507	13.947.059	17.433.824		

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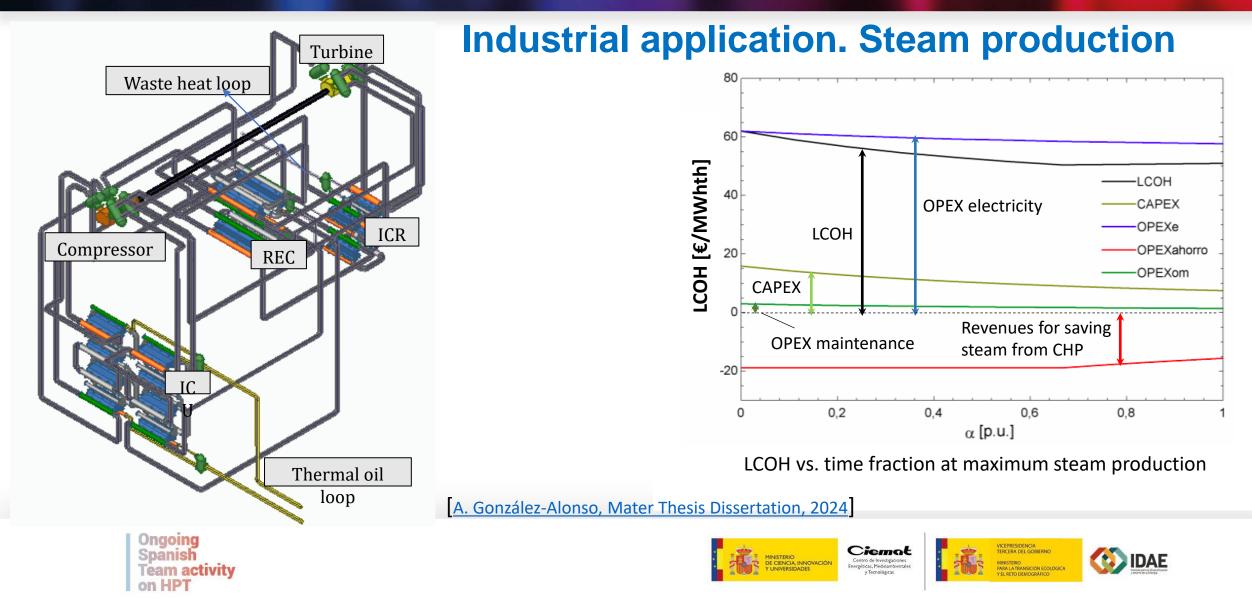
















## Conclusions

- Conventional technology does not allow to reach temperatures higher than 150 °C
- Reverse Brayton HP has revealed as a flexible system:
  - Overcomes working fluid decomposition issues associated with high temperatures
  - Uses CO<sub>2</sub>, with ODP = 0 and GWP = 1
  - Overcomes high temperature issues of reciprocating compressors
  - Suitable temperature profile (both source and sink) for fluids with temperature change:
    - Very low outlet temperatures from the waste HX, allowing the use of waste water for chilling
    - Excellent approach to maximum working fluid temperature
- Integration with thermal energy storage is possible moving the PHX to the low pressure side, enabling the use of tube/fin heat exchangers, S&T, or hybrid PCHE, able to work with molten salts or air (solid material as storage medium).
- Issues detected:
  - No commercial units with this technology
  - Only few manufacturers: Echogen, Man (Pasch)
  - Problems with scale:
    - Small units (< 2 MWth) require high speeds turbomachines. Micro-gas turbine manufacturers?
    - Large units (> 30 MWth) require large investments, but turbomachineries are commercial













### Thank you for your attention

linares@comillas.edu















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